#### Intensiv-Filter GmbH & Co. KG

## **Optimized Cleaning Systems for Industrial Baghouse Filters**

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#### **Optimized Cleaning Systems for Industrial Bag Filters** Introduction





Leadership in industrial dedusting technology for more than 85 years

#### **Optimized Cleaning Systems for Industrial Bag Filters** Introduction



#### More than 50,000 references all over the world

Process filter, kiln and rawmeal mill dedusting - France



Introduction

#### ProJet mega® PJM 136/36-8000-D

Heidelberg Cement, Cementa Slite, Gotland Sweden

Cement kiln and rawmeal mill dedusting

Turnkey project, 1,225,000 m<sup>3</sup>/h a.c.,  $c_{RG} = 300 \dots 900 \text{ g/m}^3$ 



#### During erection (July 2009)

After hot commissioning (Nov. 2009)

## INTENSIV I FILTER





Introduction



A special pressure measurement system was used to determine the efficiency of the cleaning systems for bags up to 12m length.

Introduction

#### **Comparison of different injector systems**







a) Hole type nozzle with inlet nozzle b) Ideal nozzle with inlet nozzle

c) Coanda Injector with inlet nozzle

#### **Optimized Cleaning Systems for Industrial Bag Filters** Test conditions



• Test with dust complicates the measurements and compromises the measuring technique



- Tests were performed with a special filter medium and without dust.
- Several bags from practice analyzed and the air permeability (DIN EN ISO 9237) measured

Air permeability [I/(dm <sup>2</sup> ·min)] @ 200 Pa according to DIN EN ISO 9237					
Dust loaded bags before cleaning	Bags after the jet-pulse cleaning				
4 - 6	10 - 50				



A special filter medium with 5 l/(dm<sup>2</sup>·min) was selected .



For validating the test, a filter medium with 30  $I/(dm^2 \cdot min)$  and a steel pipe with 0  $I/(dm^2 \cdot min)$  were added to the tests.

#### **Optimized Cleaning Systems for Industrial Bag Filters** Test conditions





**Test bench** 



Positioning of transmitter inside bag



Quick response pressure transmitters



**Evaluation unit** 



Software

Analysis of pressure progression inside filter bag



Analysis of pressure progression inside filter bag



#### Analysis of the impulse measurement



(Surface integral below the positive part of the bag pressure curve)

$$p_D = \int_{t_1}^{t_2} p(t) \cdot dt$$

MENS

**Test results** 



INTENSIV Imp Filter

**Test results** 



#### Minimum: about 300-400 Pa for limestone (Sievert)

**Test results** 



**Test results** 



Minimum: about 900 - 1000 Pa for limestone (inclusive under pressure of 600 Pa)



- The minimum required tank pressure for an effective dust cake release.
- Bags up to 12 m can be regenerated with the optimized Intensiv-Filter cleaning system for online and offline operation.
- The optimal cleaning pressure must be adapted individually for each application to achieve minimum energy consumption.

Because of several parameters influencing the optimal operating point of a baghouse filter and the cleaning system respectively, a new calculation tool has been developed and introduced onto the market.

# ProExpertise

#### **Optimized Cleaning Systems for Industrial Bag Filters** ProExpertise



ProExpertise						
Sprache/Language	English	Deutsch/ English				
Default Values		_				
Type of dust		Raw meal/kiln dust				
Dust concentration [g/m <sup>3</sup> ]		535	ļ			
Operating temperature [°C]		125	+_		Input	
volume flow [m*n] a.c.		830.557	Gross		Calculated	
Air-to-cloth ratio [m³(m4-min)]	accord air	0,7	rvet			
Energy demand for 1 M <sup>3</sup> (n.c.) compr fkWb/m31	essed all'	0,1				
Fan officiency		0.8	+			
Annual operating hours [h/a]		8000	-			
Floctricity rate [£/kWh]		0.05	Input-IC JN or PIM			
Filtor type		0,05 D.IM				
Number of bags per chamber		136	mput. 00, on or	r ont		
Number of chambere		130	+			
Number of chambers during cleaning	Imper of chambers		Input: 0 for Only	1		
Injector type	(onnie)	N	Input: C or N - /	~ C = Coanda and N	I – Nozzla	
Filter medium		Mombran	Input: Mombre	ProTox m Ac 7	ProTox DI	
Operating mode		Offline	Input: Offline or	Online	IVION F1	
Bag diameter [m]		0 165	input. Online or	Online		
Dag longth [m]		0,105	ł			
Tomporature of compressed air [90]		20	ł			
Safety factor (loaks and losses)		20	ł			
Air tank volume [1]		10%	-			
Filter area [m <sup>2</sup> ] (gross)		40	-			
Filter area [m <sup>2</sup> ] (gross)		10175.2	-			
Filler area (ill-) (iller)		19175,5	-			
Number of bags in total		4050	+			
Number of injection tubes per chamb	er	9	-			
Calculation Doculte		0				
		Cleaning n		1		
Cycle time [s]	0.6	0.5		03	0.2	
offic time [3]	0,0	verare pressure drop	(filter bart + f	ilter cake [Da]	0,2	
104	763	769	774	780	809	
194	105	Pressure drop (m	iscellaneous	**) [Da]	003	
104	320	320	320	320	320	
194	320	Total average r	ressure dror	[Pa]	320	
104	1193	1120	1104	1200	1220	
194	1105	Compressed air on	nsumption fr	m <sup>3</sup> /h n c l	1229	
104	1000	968	706	596	377	
194	1000	nual energy demand (e	ompreseda	ir + fan) [kWb	(a]	
104	3 530 525	3 436 013	3 318 0F2	3 237 414	3 138 321	
194	0.000.020 A	nnual operating costs	compressed	air + fan) [6/2	1	
	470 500	171.946	165 049	161 071	450.040	
10/1						

- Input of design and operating parameters, e.g. gas volume, raw gas concentration, temperature, cycle time, filter medium, bag length...
- Calculation of pressure drop and the energy demand in € of the filter plant.
- ProExpertise validated by several filter plants in practice.

#### **Optimized Cleaning Systems for Industrial Bag Filters** ProExpertise



Operating costs of a filter plant (without filter bag costs):





## www.intensiv-filter.com

## Thank you for your attention.